

Two phase anaerobic digestion

Bernd Linke
Leibniz-Institute for Agricultural Engineering
www.atb-potsdam.de

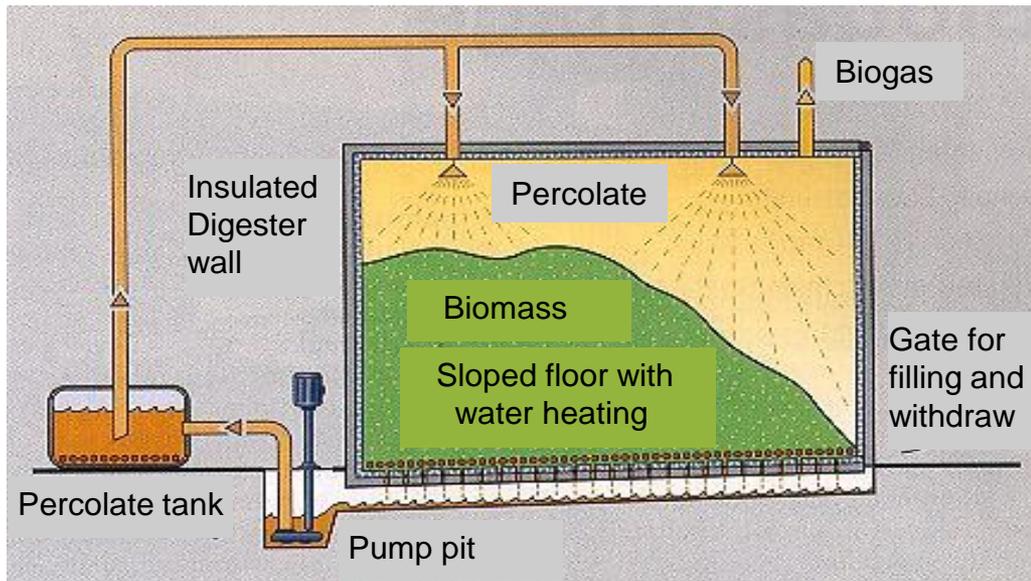
- Brief description of two-phase systems
- Case study BioFerm/ Vissmann Group
- Batch operation experiments
- Continuously operation experiments
- Advantages of Two-phase systems

Brief description of two phase systems

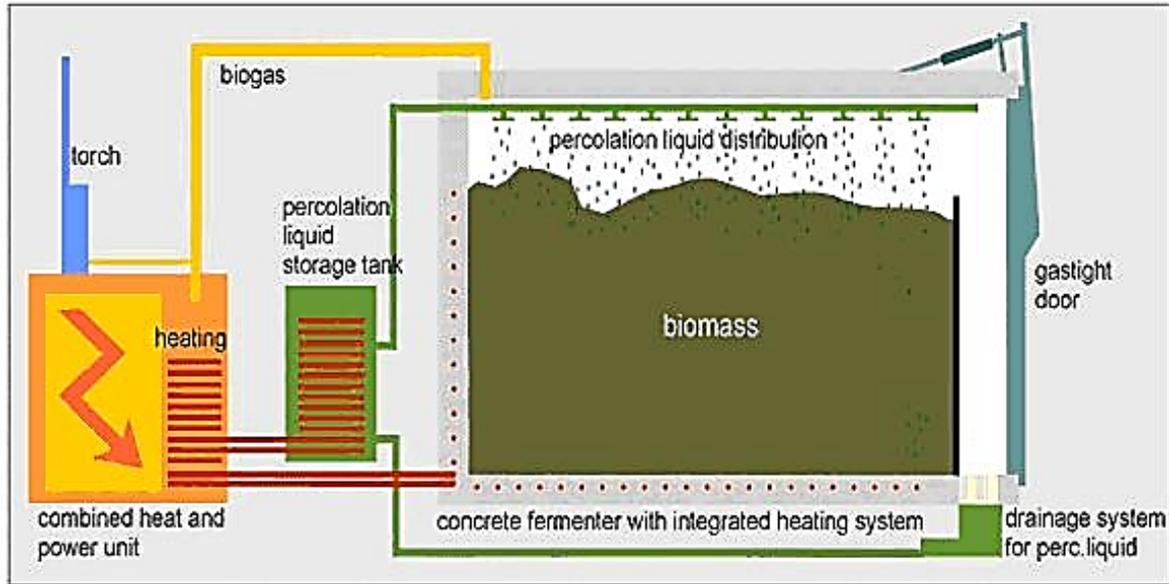
Anaerobic Digestion (AD) for structural biomass, Percolation of biomass (solid phase) by means of a liquid phase with low parasitic energy consumption due to the lack of moving parts

- **Process A (batch):** Mixing of digested material (inoculum) with feed, percolation for 20 – 40 days,
- **Process B (batch):** Percolation of feed without inoculum for 20 – 40 days, degradation of VFA in a methane reactor
- **Process C (continuously):** Percolation in a floating bed digester, (Biomass lift up), degradation of VFA in a methane reactor at high OLR

Two phase, one step, Bioferm/Vissmann Group Biomass with inoculum (Process A)



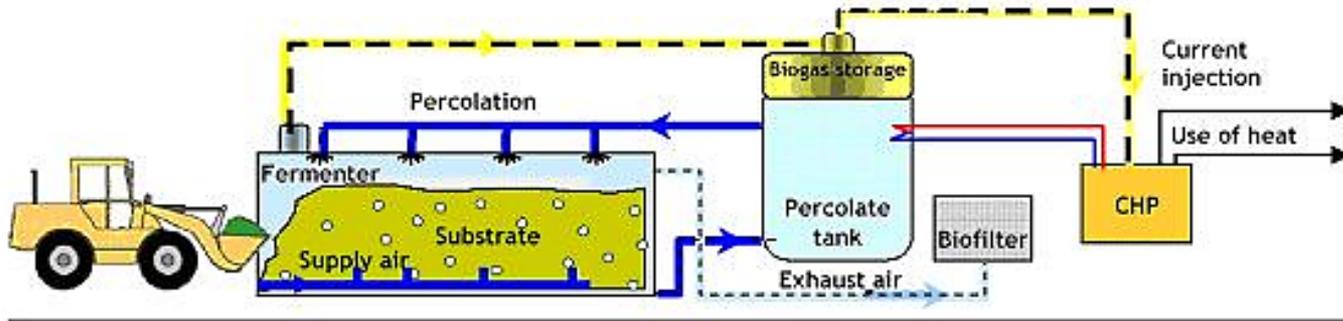
Two phase, one step, Bekon Technology Biomass with inoculum (Process A)



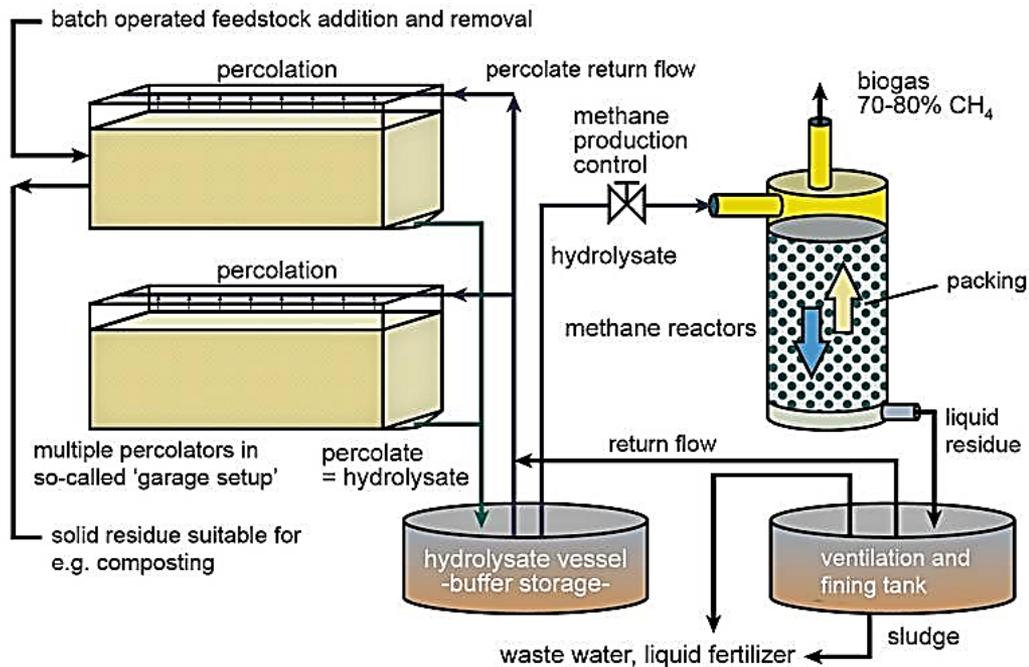
BEKON
Energy Technologies GmbH & Co. KG



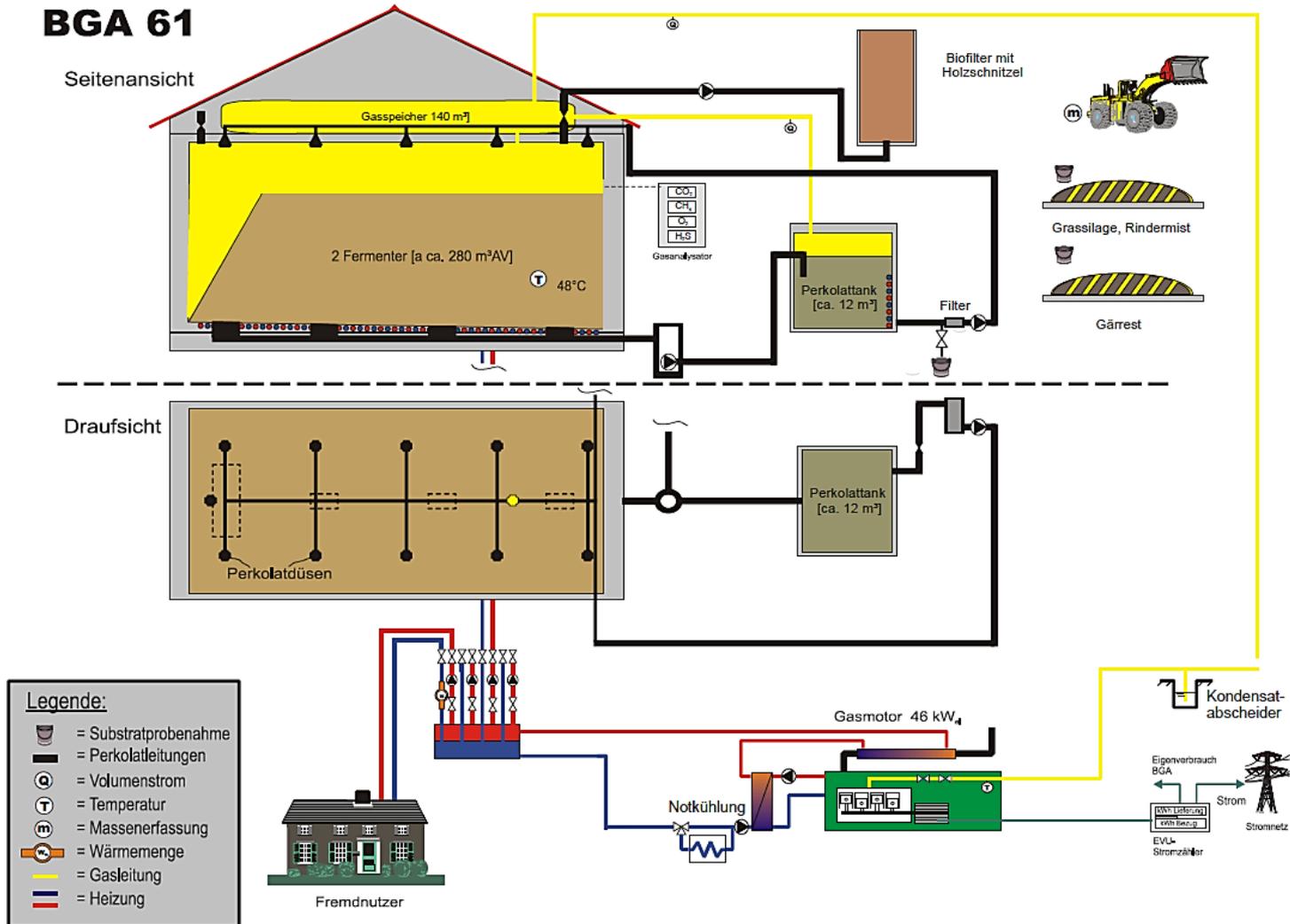
Two phase, one step, Loock Biogas systems Biomass with inoculum (Process A)



Two phase, two steps, Gicon Technology Biomass without inoculum (Process B)



Case study BioFerm/ Vissmann Group (A)



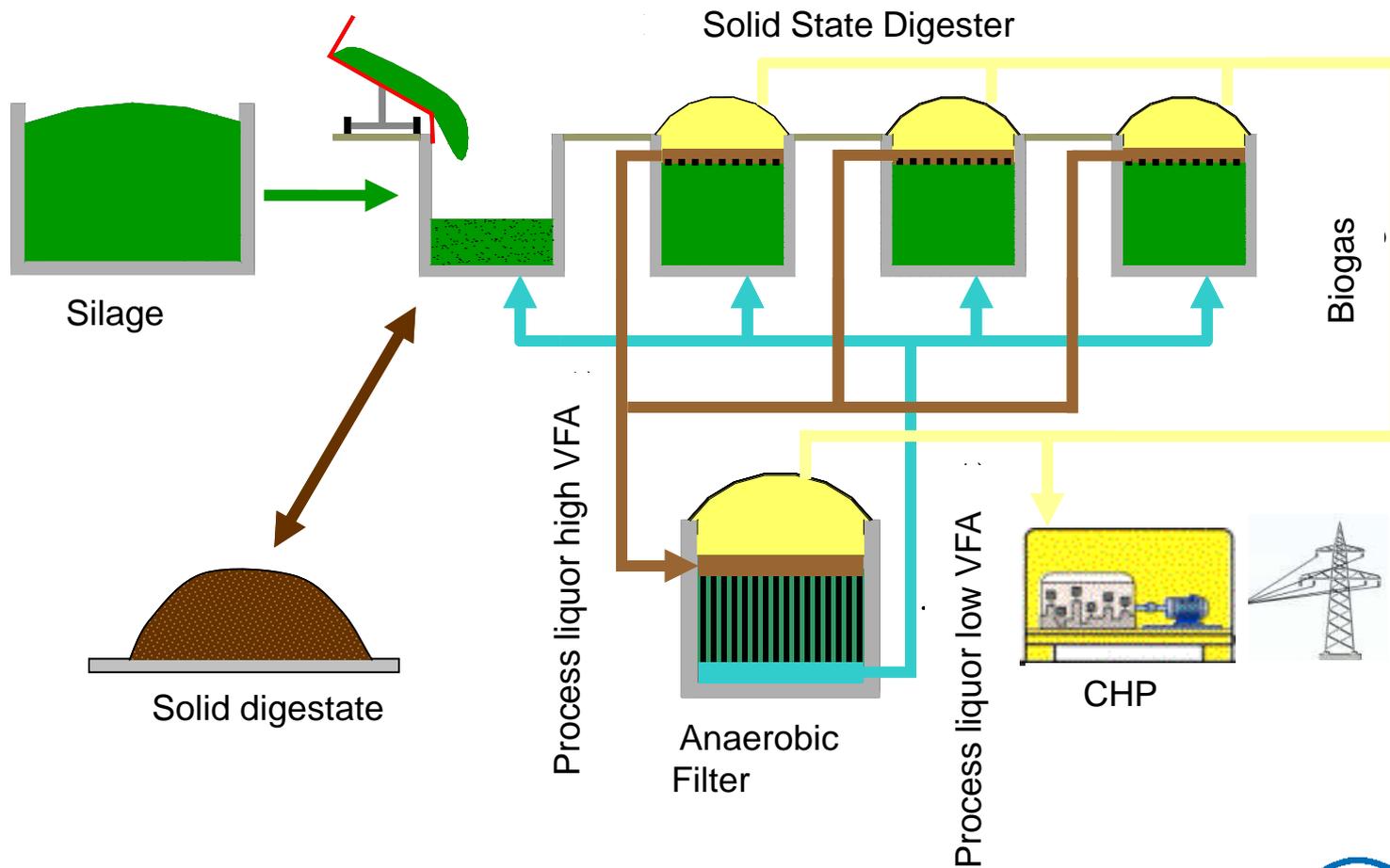
Case study BioFerm/ Vissmann Group (A)

Parameter	Data
Farm data	5 ha cropland, 125 ha grassland, 70 sheep, 12 cows
Substrate feed	1034 t/a, 52% grass silage, 31% fresh grass, 14% cattle manure, 3% hay, % fresh mass (FM)
	TS = 37% FM, VS = 33% FM, $\text{NH}_4\text{-N} = 1\text{kg t}^{-1}$, $\text{N}_{\text{tot}} = 9.9\text{ kg t}^{-1}$
Digester	2 digester each 408 m ³ , 1 percolation tank 12 m ³
Digester operation	Residence time 18 days, proportion of digestate in the mixture 39% FM, T = 48°C, pH = 7.6, OLR = 1.9 kgVSm ⁻³ d ⁻¹ . Ac = 1.7 kg t ⁻¹

Case study BioFerm/ Vissmann Group (A)

Parameter	Data
Digester performance	VS-biogas/methane yield $y = 309/155 \text{ m}^3\text{t}^{-1}$ (54.3% CH_4) biogas/methane productivity $R = 0.57/0.29 \text{ m}^3\text{m}^{-3}\text{d}^{-1}$
Digestate quality	TS = 23.6% FM, VS = 15.7% FM, $\text{NH}_4\text{-N} = 1.2 \text{ kgt}^{-1}$, $\text{N}_{\text{tot}} = 7.2 \text{ kgt}^{-1}$ Residual methane yield (20°C, 60 days) $5.4 \text{ m}^3\text{t}^{-1}$ FM
Biogas utilisation	CHP (46 kW_{el}); 364 KWh_{el} /day, current sale in power grid, 1368 KWh_{th} /week heat utilisation, replacement of fossil fuels

Two phase, two steps, Experimental plant



Two phase, two steps, Lab-scale

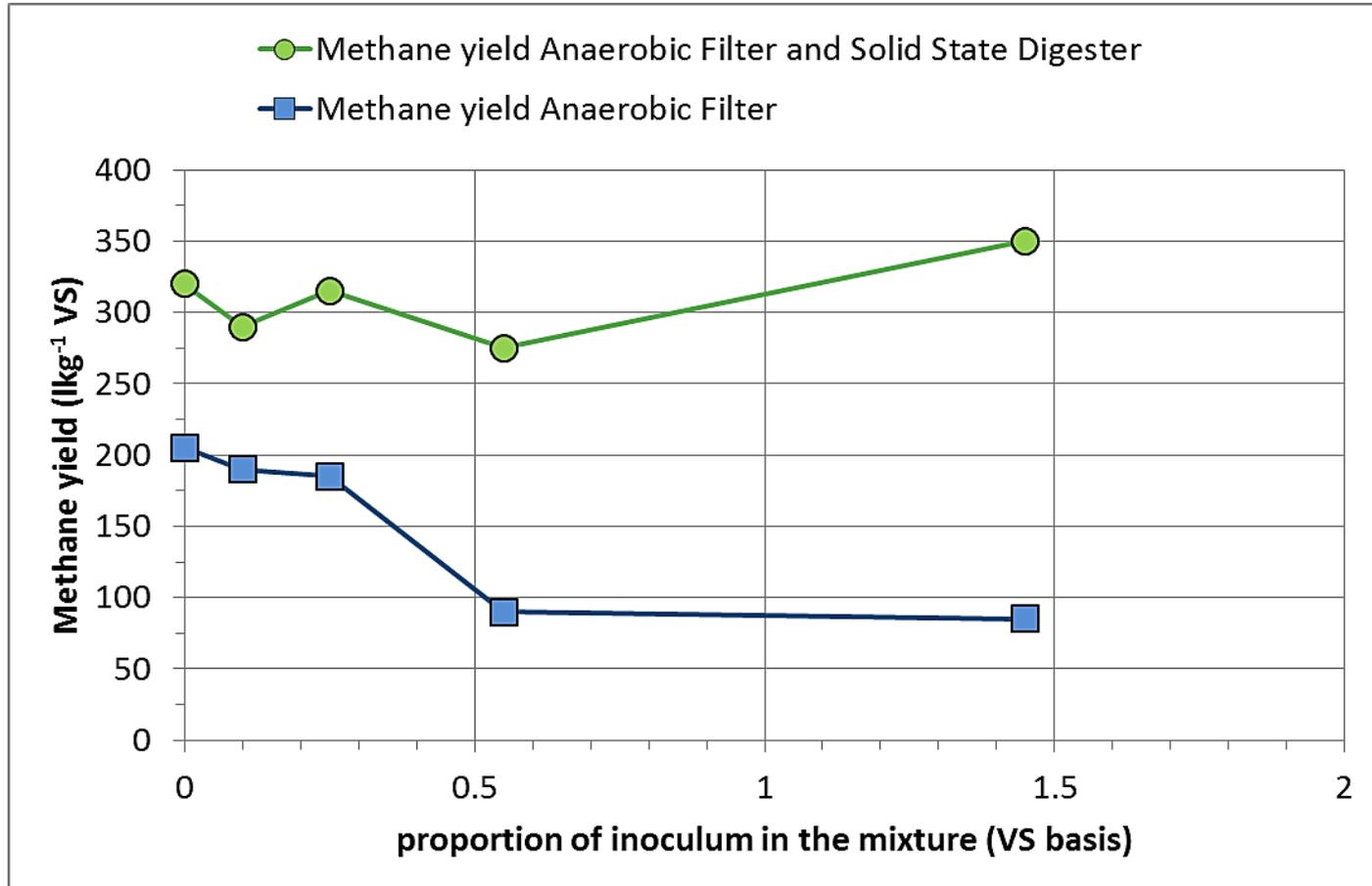
peristaltic pumps

Fixed film digester (FFD 50L)

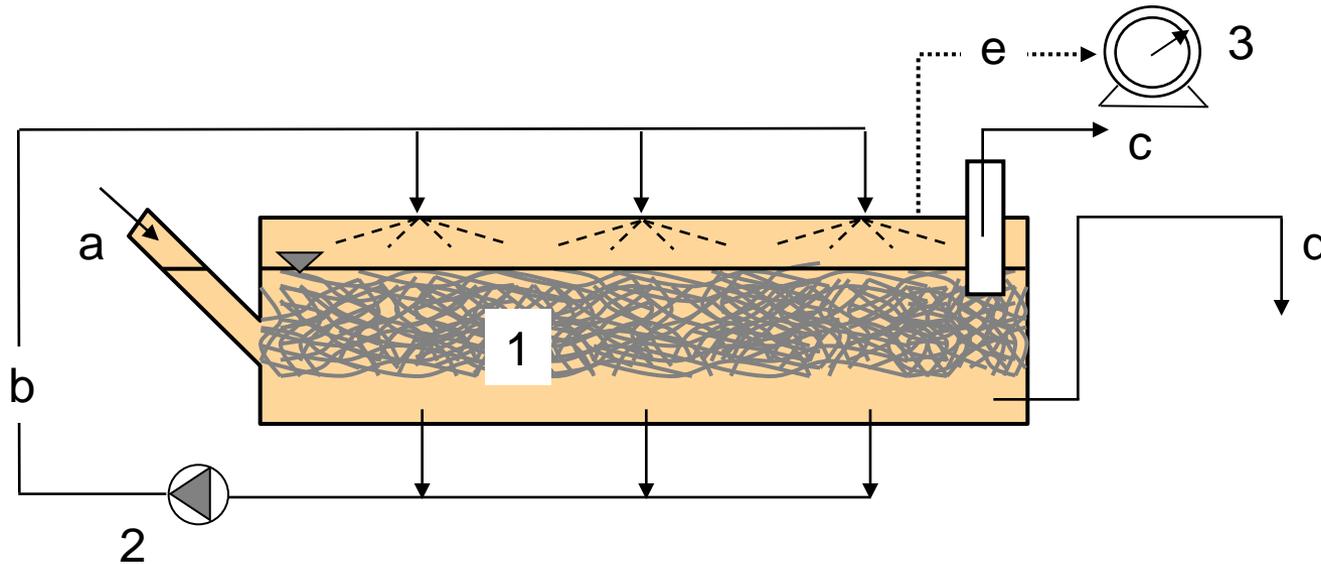


Solid state digester (SSD 50L)

Methane yield as function of inoculum proportion (whole crop silage)



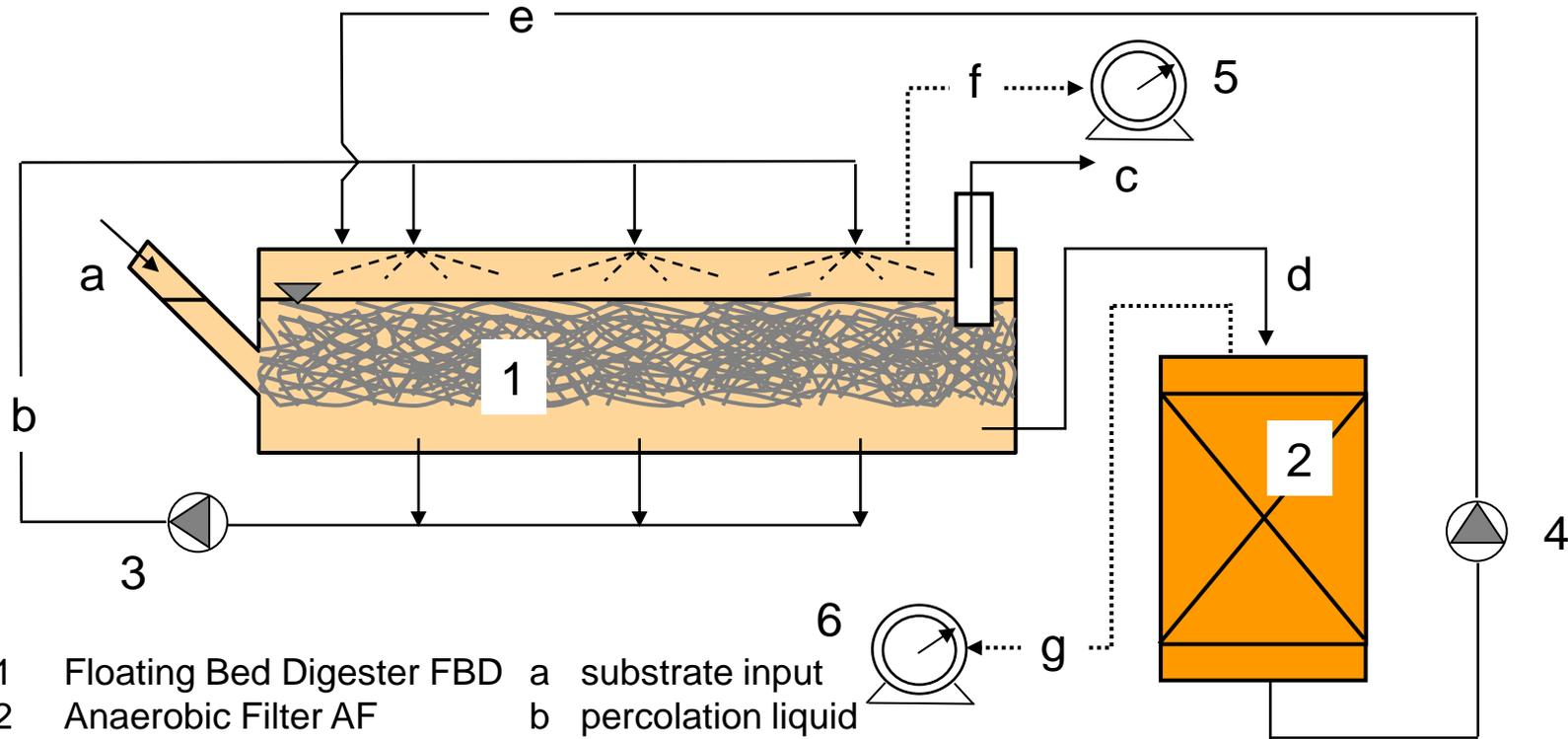
Continuously fed 540 L Floating Bed Digester (FBD)



- 1 Floating Bed Digester FBD
- 2 peristaltic pump
- 3 wet gas meter

- a substrate input
- b percolation liquid
- c solid digestate
- d liquid digestate
- e biogas

Continuously fed Floating Bed Digester (FBD, 55L) coupled with 40 L Anaerobic Filter (AF 40L)



- | | | | |
|---|---------------------------|---|--------------------|
| 1 | Floating Bed Digester FBD | a | substrate input |
| 2 | Anaerobic Filter AF | b | percolation liquid |
| 3 | peristaltic pump FBD | c | digested material |
| 4 | peristaltic pump AF | d | influent AF |
| 5 | wet gas meter FBD | e | effluent AF |
| 6 | wet gas meter AF | f | biogas from FBD |
| | | g | biogas from AF |

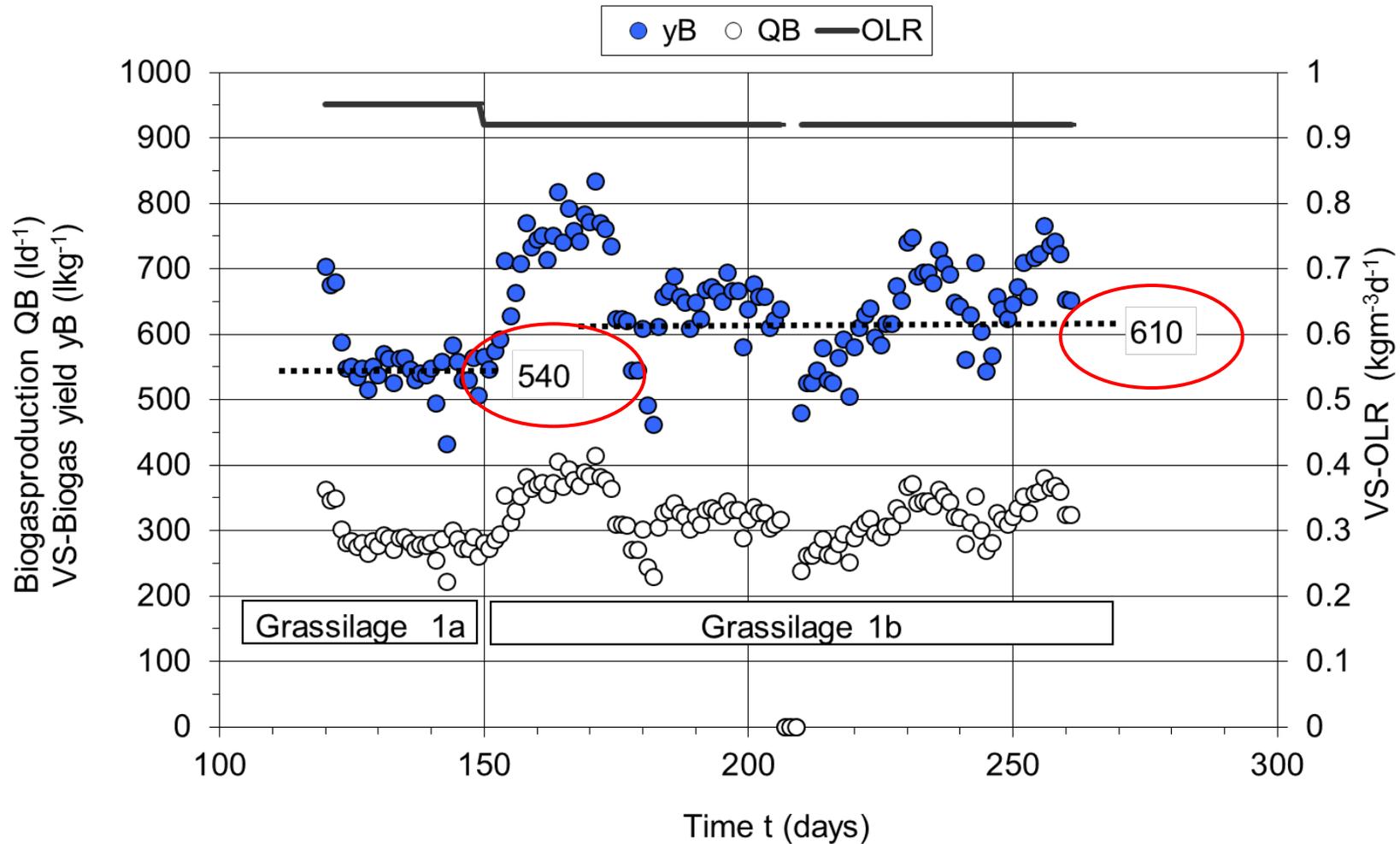
Analysis of Feed-Gras Silage

Feed	pH	TS	VS	Raw Fibre	Sugar	N _{tot}
	-	% FM	% TS	% TS	% TS	% FM
Grassilage 1a*	5.1	55.6	92.4	35.2	2.0	1.25
Grassilage 1b*	5.2	53.0	93.7	32.2	9.8	1.12
Gassilage 2**	4.2	36.0	90.9	30.0	3.1	1.08

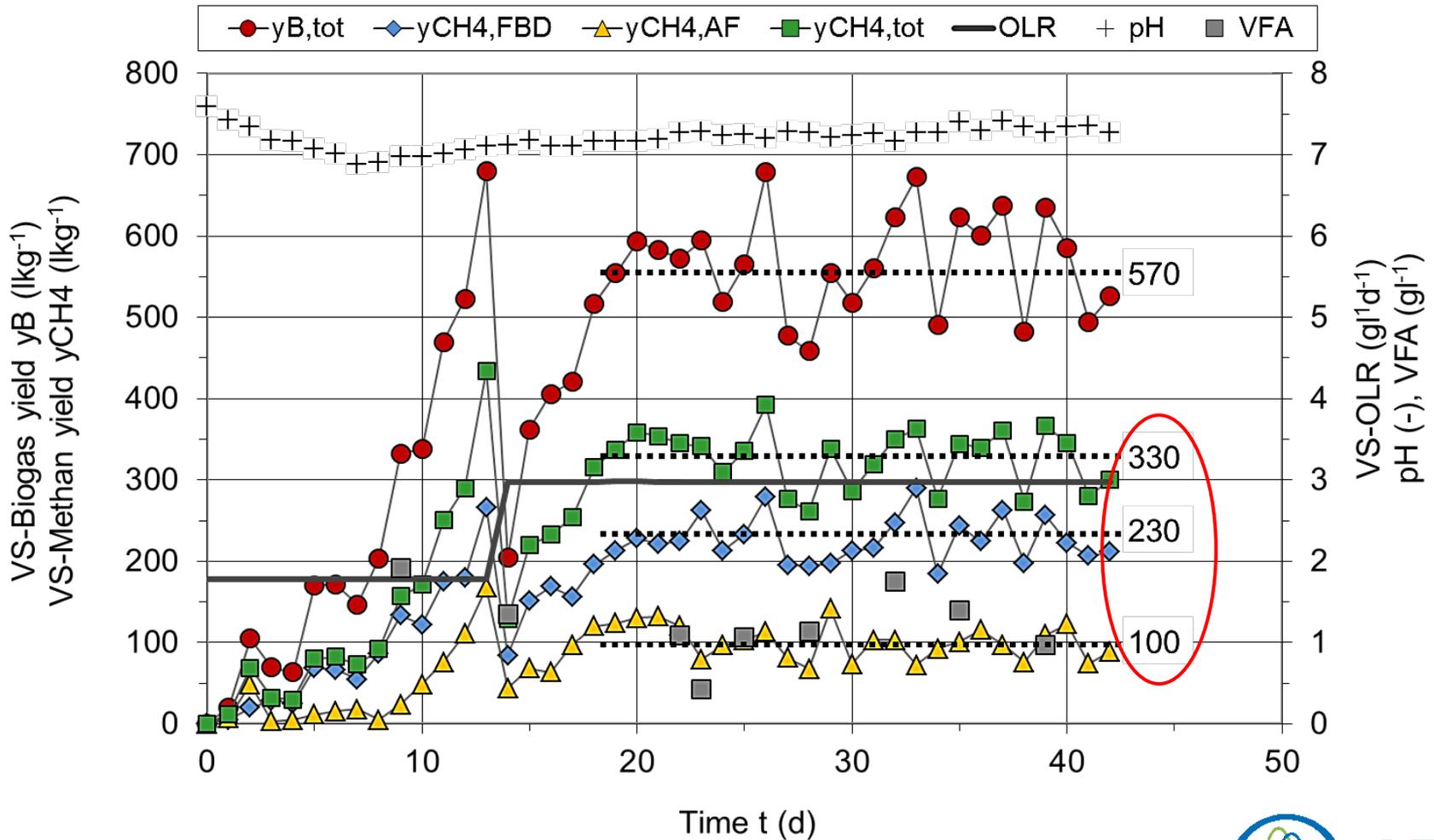
* Feed used for FBD (540 L) trials

* Feed used for FBD (55L) with AF (40L) trials

Results from 540 L Floating Bed Digester (FBD)



Results from Floating Bed Digester (FBD, 55L) coupled with 40 L Anaerobic Filter (AF 40L)



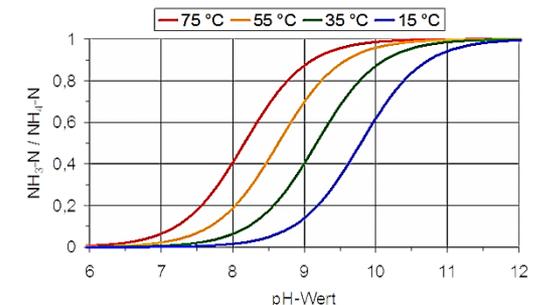
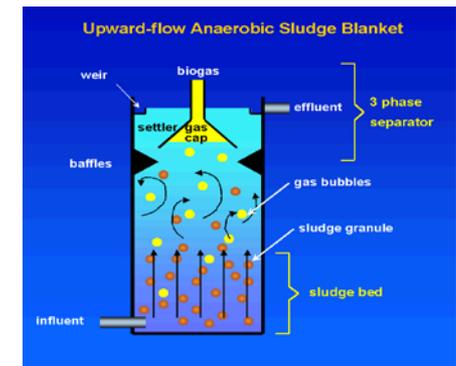
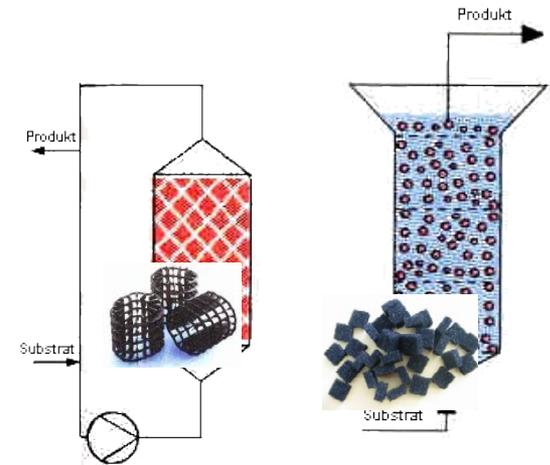
Treatment of process liquor for VFA degradation

- High performance digesters with biomass retention for degradation of VFA and soluble organic compounds → inhibition at low pH-value

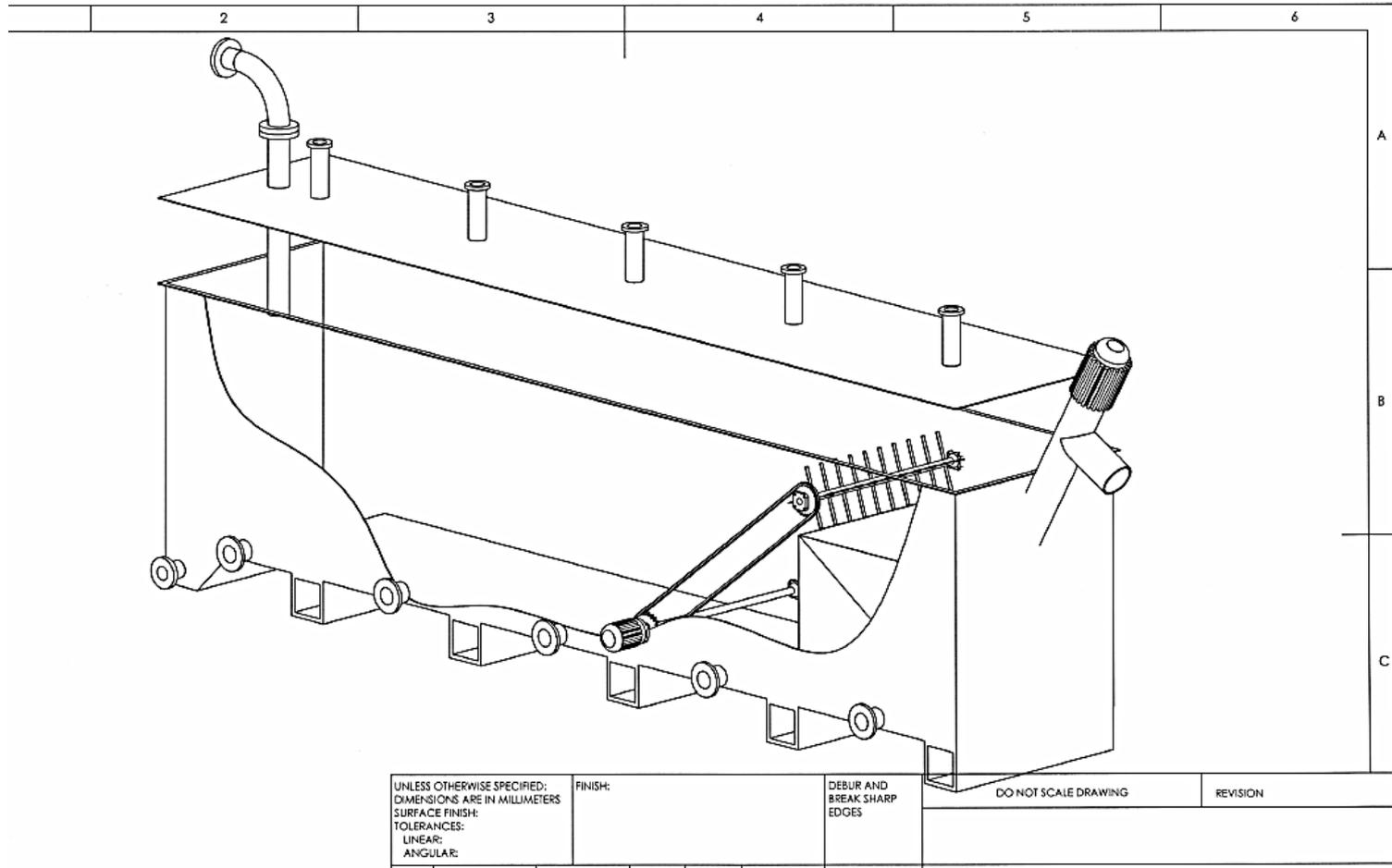
- Anaerobic filter digester
- Fluidized bed digester
- UASB digester

- Removal of Ammonia → inhibition at high pH-value

- Desorption (stripping) of NH_3 by means of air, steam at low pressure
- Precipitation of NH_4 by adding of MgCl_2 and $\text{H}_3\text{PO}_4 \rightarrow \text{MgNH}_4\text{PO}_4$ (Struvit)



Draft of a FBD



Thank you
for your attention!

