Processing of Digestate

Project of BFE October 2011 – summer 2013

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for large biogas plants, digestate has to be transported great distances for utilisation

transport of water needs energy

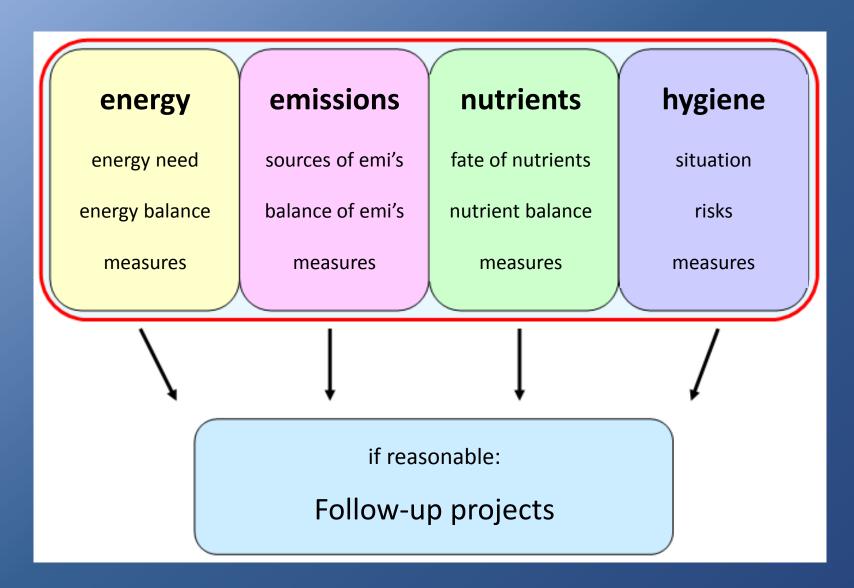
 is it reasonable to separate nutrients, notably N, from an energetic and ecological point of view?

are there additional advantages of nutrient separation?





Modules of the Project



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Digesters



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Solid/liquid separation



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Ultra Filtration



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Reverse Osmosis

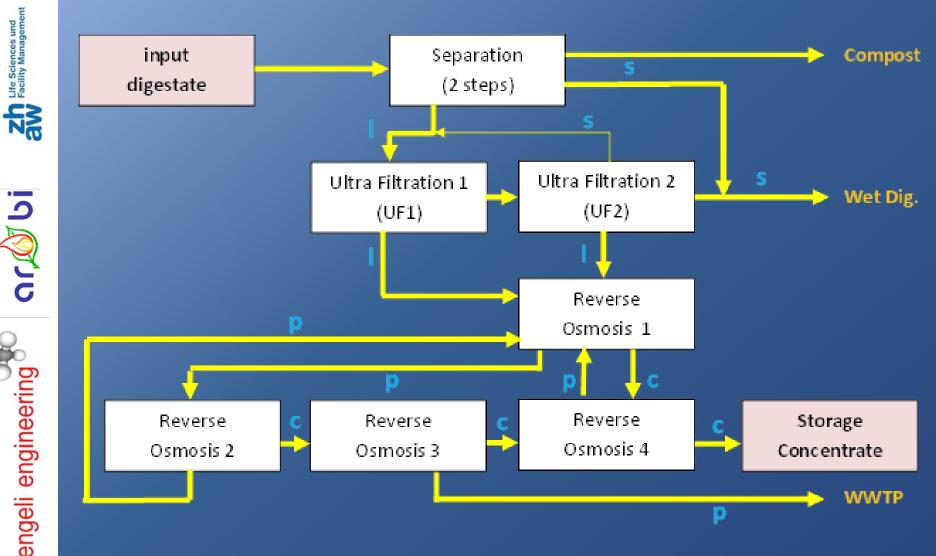


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the digestate processing plant









Module Energy

energy needs of the single steps

energy need compared to energy output

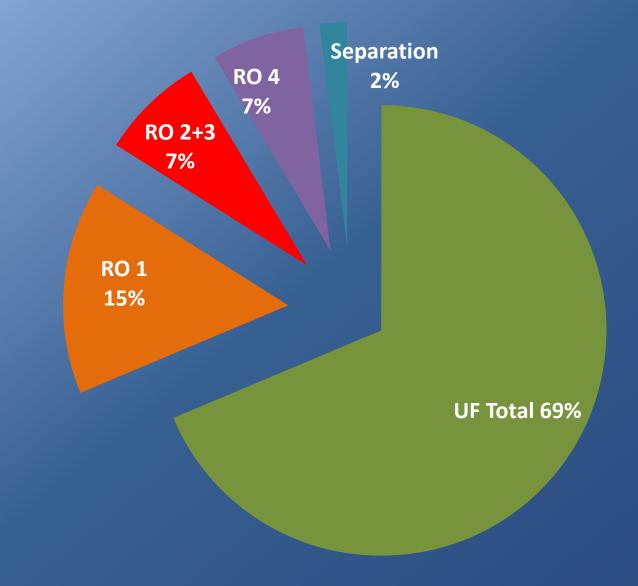
savings of fossil fuel for transportation

comparison of energetic costs and benefits

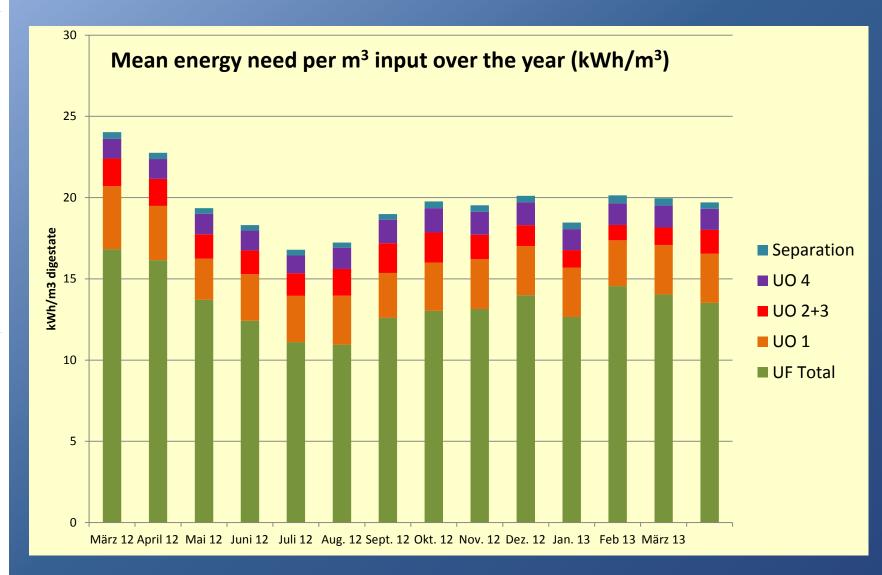
are there savings of chemical fertilizers by separating the nutrients?

Energy need of components





Seasonal energy need

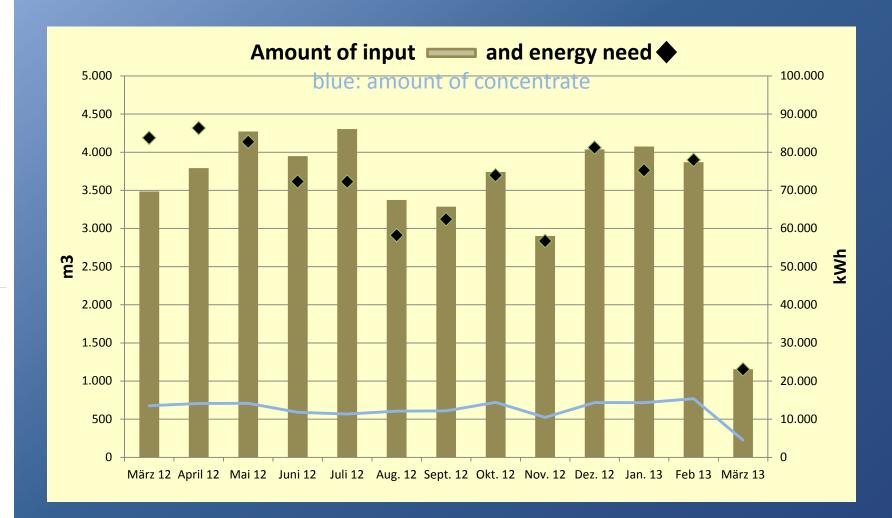


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Energy need and amount treated



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Energy produced and energy needed for processing

Mean yield of Biomethane (H _s) per fresh material	405	kWh/t
Electricity produced (η = 38%)	154	kWh _{el} /t
Energy need for processing of the digestate	22.5	kWh/m ³
Percentage of H_s needed for processing	5.5	%
Percentage of the electricity produced needed for processing	14.6	%

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Module Emissions

three sources of emissions:

emissions from the plant itself while processing the digestate

emissions of the trucks while transporting and delivering the liquid fractions

gaseous emissions while applying the fertilizer on the field

Emissions from the plant

between delivery and digestion: identical emissions

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s/l-separation: ev. less as compared to agri digester

no emissions from UF and RO

emissions from storage of concentrate comparable to those, when storing liquid from l/s-separation (higher concentration in the head space – but less respiration)

> conclusion: no significant difference to a conventional plant







Emissions from transportation

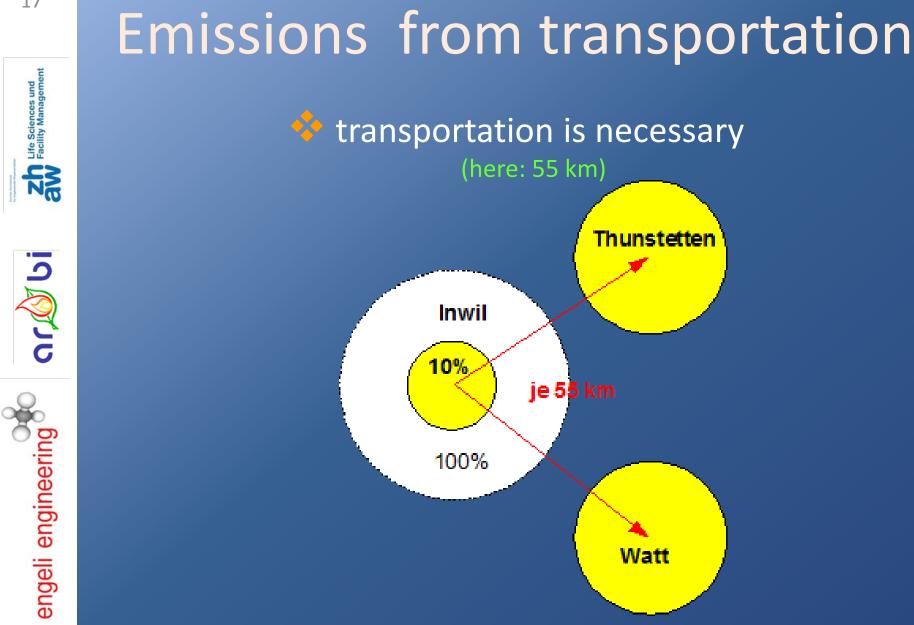
transportation is necessary (here: 55 km)

transport to the fields are reduced by a factor of 3

drilling of concentrate doubles the ride on the field

drilling needs 2-3 times more energy than a draghose

final results: after experiments! (probably no big advantage)









Emissions while applying

pH of concentrate = ~ 8.1-8,3 !
(~ 10% of the Ammonium-ions are converted into Ammoniac!)

high risk of ammonia losses

Dutch studies indicate that losses are difficult to avoid

conclusion: field experiments and experiments on plots will be done next month (collaboration with BHL)







Module Nutrients

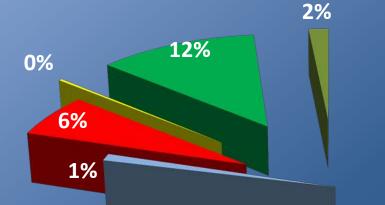
questions:

distribution of nutrients and heavy metals in the different fractions of digestate separation

mass balances of DM and OM

are there possibilities for an optimization?

e.g.: fate of OM



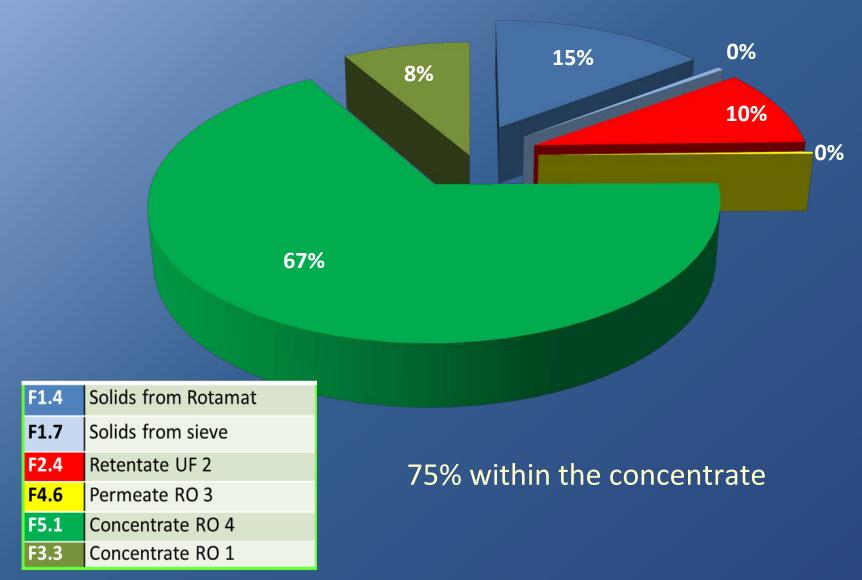
F1.4	Solids from Rotamat
F1.7	Solids from sieve
F2.4	Retentate UF 2
F4.6	Permeate RO 3
F5.1	Concentrate RO 4
F3.3	Concentrate RO 1

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79%

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e.g. Fate of Ammonium

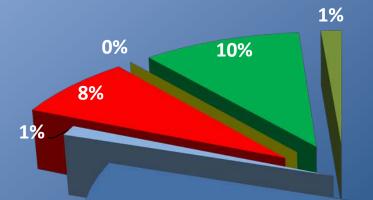


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e.g. fate of Phosphorus



F1.4	Solids from Rotamat
F1.7	Solids from sieve
F2.4	Retentate UF 2
F4.6	Permeate RO 3
F5.1	Concentrate RO 4
F3.3	Concentrate RO 1

Mainly within solid fractions (like also heavy metals)

80%

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Module Hygiene

project in collaboration with FIBL: testing Salmonella, coliforme sperms, E. Coli, Enterococcus

input shows partially high contaminations, especially biowaste with food waste (10⁶-10⁷)

no germs could be detected in the storage of «liquid» fraction after separation, in front of and after UF

> further measurements necessary (n=1)





nutrient processing will probably only play a role in specific, well defined situations with high cattle densities

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So: keep in mind! Produce biogas from waste, as simple as possible!



Thanks for your attention!

Hans Engeli, engeli engineering

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